


VAL-MATIC®


**Pump Control Ball Valve
for Energy Savings**



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PUMP CONTROL BALL VALVE FOR ENERGY SAVINGS

INTRODUCTION

An essential element in the design of water and wastewater pumping systems is the proper selection of the pump control valve, whose primary purpose is prevent reverse flow when the pump is not in operation. A pump control valve must also be able to carefully and slowly control changes in fluid velocity to prevent water hammer or surges, especially in long pipelines. Another function that is often overlooked is the valve's ability to minimize energy consumption. It is estimated that water and wastewater plants consume nearly 80% of their costs to pump water and overcome pressure and friction losses. By proper valve selection to minimize valve headloss, significant energy savings can be achieved.



FIGURE 1. Pump Control Ball Valves in Ohio, USA

There are several types of pump control valves including butterfly, ball, and eccentric plug valves, which are electrically wired to the pump control circuit to provide synchronized functions with the pump to systematically control the changes in pipeline fluid velocity over a long period of time (i.e. 60 to 300 seconds) to prevent surges in pipelines, force mains, and

distribution systems. When selecting a pump control valve, you should consider performance, low headloss, and flow characteristics. This paper will therefore describe the advantages of using AWWA C507 ball valves for pumping applications.

PUMP CONTROL VALVES

When pumping systems are part of very long piping systems (i.e. 20,000 ft), pump control valves are required to control water hammer or pressure surges. Pump control valves are typically quarter-turn valves equipped with slow opening and closing electric motor or hydraulic cylinder actuators. The actuator is powered by an external electric or pressure source and must be electrically connected to the pump circuit for control purposes. The motion of the closure member in these valves is controlled by the power actuator so they are not subject to fluttering or slamming like automatic check valves. Further, because the actuator rigidly restrains the closure member, there is no need for three to five straight diameters of pipe upstream of the valve as with swing check valves. Battery systems or pressurized accumulator systems can be used to enable the pump control valve to close after a power failure. Alternatively, an automatic check valve such as an AWWA C508 Check Valve with low headloss can be used (see Figure 2) to prevent reverse flow after power failure. Finally, quarter-turn valves are designed to handle high fluid velocities (up to 16 ft/sec) so are often sized to be smaller than the pump discharge to provide improved flow characteristics.

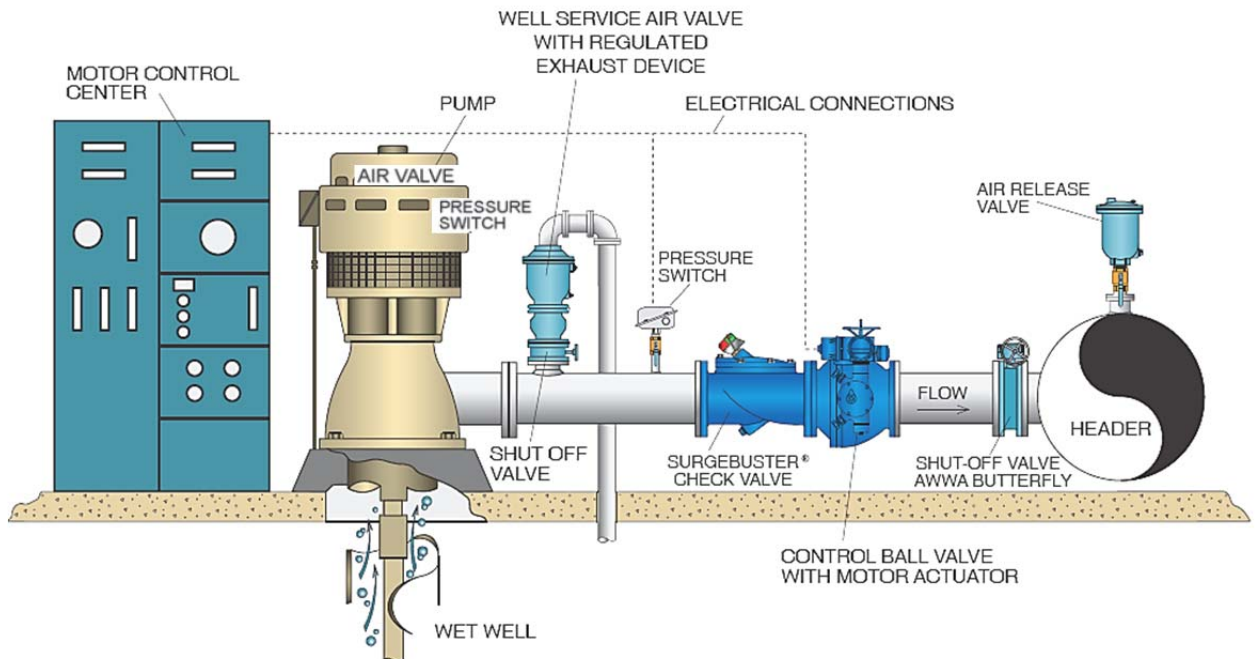


FIGURE 2. Typical Pump Control Ball Valve

Figure 2 illustrates a pump control ball valve installation. The ball valve is operated by rotating its shaft and closure member 90 degrees and is equipped with an electric motor

actuator sized to operate the ball valve very slowly in five minutes. This ball valve is backed up by an AWWA C508 Check Valve for when all electrical power is lost. The ball valve works in harmony with the pump motor control center. When the pump is signaled to START, the pump develops pressure and a pressure switch signals the ball valve to slowly open. When the pump STOP signal is given, the ball valve closes, but the pump continues to run. When the ball valve is closed, or near closed, a limit switch signal from the valve actuator is given to the pump to STOP.

This process assures that changes in fluid velocity from pump operation happen very slowly over several minutes thereby preventing surges. However, when there is a power failure, the pump will stop in a few seconds and to prevent excessive backspinning, the pump control ball valve will close quickly in 5 to 10 seconds. This sudden closure of the pump control or check valve after power failure may cause a pressure surge, so surge relief equipment such as surge tanks or pressure relief valves are sometimes used. Because of the complexity of the pump inertia, valve closure, and pipeline hydraulics, a computer transient analysis is employed to verify that excessive surges will not occur.

HEADLOSS

The pump discharge head is needed to overcome the combination of the static head and the friction head of the distribution system. The static head represents the difference in elevation between the source and the highest point of water storage or service. The friction head is caused by roughness in the pipe and local flow disturbances such as fittings and valves. Pumping and distribution system valves come in many varieties, but they all cause some friction head.

Valve body geometry dictates the general flow area through the valve. Some control valves restrict the flow area to below 80% of the pipe area. Also, the internal contours of the body and seat should be smooth to avoid creating excessive turbulence. The design of the closure member is also important in reducing headloss. The lowest headloss will be achieved if the closure member rotates out of the flow path. The ball valve has the lowest headloss because when the valve is open, the flow path is the same as a straight length of pipe.

There are many flow coefficients and headloss formulas in general use today for rating various valves on the basis of headloss. Probably the most common flow coefficient for water valves is the C_v flow coefficient, which is defined as the amount of water in gallons per minute (gpm) that will pass through a valve with a 1 psi pressure drop. Hence, the more efficient the valve, the greater the valve C_v . C_v should only be used for computing headloss, not stating the valve's flow capacity. Table 1 illustrates typical flow coefficients for 12 inch pump control and check valves in order of increasing C_v .

Typical 12 in. Valve Flow Data			
TYPE OF VALVE	PORT SIZE	C_v	K_v
MSS SP125 Silent Check Valve	100%	2480	3.00

AWWA C508 Swing Check	80%	3390	1.60
AWWA C517 Plug Valve	80%	4770	0.81
AWWA C504 Butterfly Valve	90%	6550	0.43
AWWA C507 Ball Valve	100%	22,800	0.03

TABLE 1. Valve Types and Flow Coefficients

Another flow coefficient to use for making comparisons is the resistance coefficient K_v used in the general valve and fitting flow formula:

$$\Delta H = K_v v^2 / 2g$$

Where:

ΔH = headloss, feet of water column

K_v = resistance coefficient (valve), dimensionless

v = fluid velocity, ft/sec

g = gravity, ft/sec²

The flow factor K_v can also be related to the C_v by the formula:

$$K_v = 890 d^4 / C_v^2$$

Where:

d = valve diameter, in.

Finally, the flow conditions of the system can affect the valve headloss. From the ΔH equation, it is clear that headloss is a function of fluid velocity squared. Hence, a doubling of the line velocity will increase the pipe, fitting, and valve head losses four-fold. This is why pump discharge velocities are usually designed for 8 to 10 ft/sec fluid velocity and long pipeline velocities, 4 to 6 m/sec. There is an optimum pipe size and velocity that provides the least installation costs and annual operating costs.

ENERGY COSTS

Energy costs represent the consumption of kilowatt hours of electricity with a typical cost of about \$ 0.08 per kW-hr. The headloss from valves can be converted into an annual energy cost related to the electrical power needed by the pump to overcome the additional headloss from the valve with the equation:

$$A = (1.65 Q \Delta H C U) / E$$

Where:

A = annual energy cost, \$ per year

Q = flow rate, gpm

ΔH = head loss, feet of water

C = cost of electricity, \$/kW·hr

U = usage, percent x 100 (1.0 equals 24 hours per day)

E = efficiency of pump and motor set (0.80 typical)

For example, the difference in headloss between a 12 in AWWA ball valve ($K = 0.03$) and a silent check valve ($K = 3.00$) in a 3500 gpm or 9.93 ft/sec system can be calculated as follows:

$$\begin{aligned}\Delta H &= (3.00 - 0.03) (9.93)^2 / 2 \cdot 32.2 \\ &= 4.55 \text{ feet of water column}\end{aligned}$$

This difference in headloss can then be used to calculate the difference in annual operating costs assuming an electricity cost of \$ 0.08 per kW-hr. and 50% usage.

$$\begin{aligned}A &= (1.65 \times 3500 \times 4.55 \times 0.08 \times 0.5) / (0.8) \\ &= \$ 1314\end{aligned}$$

The calculation shows that the use of a 12 in ball valve in the place of a 12 in silent check valve can save \$1314 per year in energy costs. If the pump station had four such valves operating for 20 years, the total savings would be \$105,100 every 20 years. It is clear that the pumping costs can be more significant than the installed costs of the valves. Further, the larger the valve, the greater the impact from the energy costs.

FLOW CHARACTERISTICS

When the fluid velocity is changed in a steel piping system, the kinetic energy of the fluid can generate high surge pressures equal to about 50 psi for every 1 ft/sec of sudden velocity change. The pressure spike causes the noise that shakes the pipes in a building when a valve is quickly closed. In piping systems, the surge pressure travels along the pipeline and is reflected back to the pump. This time period, often called the “critical period”, can be calculated by the equation:

$$t = 2 L / a$$

where:

$$t = \text{critical period, sec}$$

$$L = \text{length of the pipe, ft}$$

$$a = \text{speed of the pressure wave, ft/sec}$$

For a 12 in pipeline, the critical period would be as follows for a 4 mile long steel pipeline:

$$t = 2 (21,120 \text{ ft}) / (3500 \text{ ft/sec})$$

$$t = 12 \text{ sec}$$

Surprisingly, any change in velocity that occurs within the critical period is the same as if it occurred instantaneously. Hence, when a pump is started and stopped in a long piping system, its 6 ft/sec change in velocity will automatically cause a surge equal to about 300 psi,

which is added to the static pressure. Such a pressure is likely beyond the safe operating pressure of the system so a surge control strategy will be required.

Typical surge strategies can include multiple pumps, surge tanks, relief valves, variable speed pumps, pump control valves, or some combination of the above. When a pump control valve is used as the check valve, its flow characteristic contributes significantly to its effectiveness. The most desirable flow characteristic of a valve is one where the valve uniformly changes the flow rate when installed in the system.

The flow data typically published by valve manufacturers are inherent flow characteristics usually expressed in terms of the flow coefficient (C_v) at various positions. By assuming a constant pressure drop of 1 psi across typical valves at all positions, the inherent characteristics of the valves can be compared as shown in Figure 3. On the left side is a quick-opening valve curve (such as a gate valve or swing check valve), which depicts a rapid change in the flow rate as the valve opens. On the other extreme is an equal percentage valve (such as a ball valve), which changes the flow rate uniformly with valve travel. However, these readily available curves only consider the valve headloss and ignore the system headloss. Inherent curves may be misleading when selecting a valve for a pumping system with long pipelines.

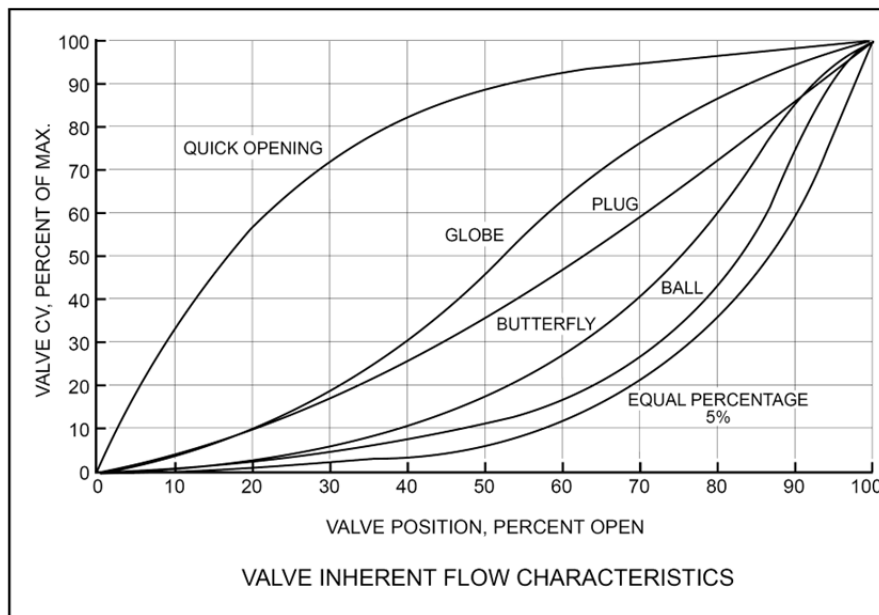


FIGURE 3. Inherent Flow Characteristics

The inherent characteristic curves must be transformed for a given pipeline application to consider the relative headloss of the piping system. So when a valve such as a ball valve is installed in a pipeline, the location of the curve varies with the length of the pipeline as shown in Figure 4. The curve shown on the right is the inherent flow characteristic curve because the system is zero feet long. The other curves are installed flow characteristic curves because they vary with the system length. As the length of the pipeline increases, the characteristic curves for the same valve shifts to the left. Hence, the same valve can be very close to equal-percentage in one system and quick-opening in another.

The longer the pipeline, the more the valve tends to be quick-opening. A quick-opening valve will change the flow suddenly and is more apt to cause surges because it effectively controls the flow for only one half of its travel. Ideally, the most desirable installed flow curve for a pumping system is linear such as the curve in the middle. Therefore, since inherent curves shift to the left when the system is included, the valve with an equal percentage inherent curve is the most desirable. Referring again to Figure 3, the most desirable valve for a long systems would be an equal percentage ball valve.

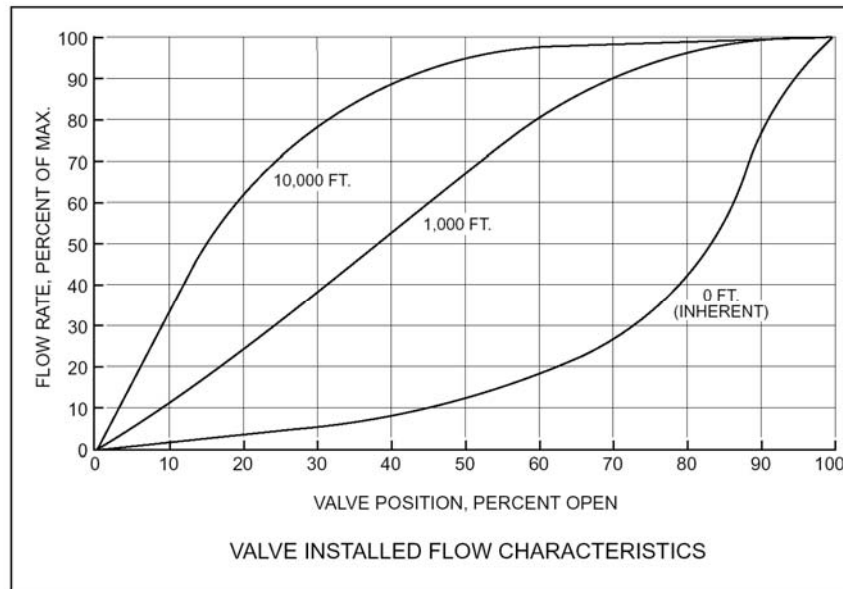


FIGURE 4. Installed Flow Characteristics

But the flow curves can also be affected by size in addition to type. For example, installing an 8 in valve in a 12 in system will shift the curve back to the right as shown in Figure 5. The shift is logical because an 8 in. valve will decrease the flow more rapidly than a 12 in. valve in the same system. So when selecting a valve, the size and its maximum flow velocity is as important as the type. Ball valves are commonly smaller than line size because of their low head loss and ability to operate at velocities up to 35 ft/sec.

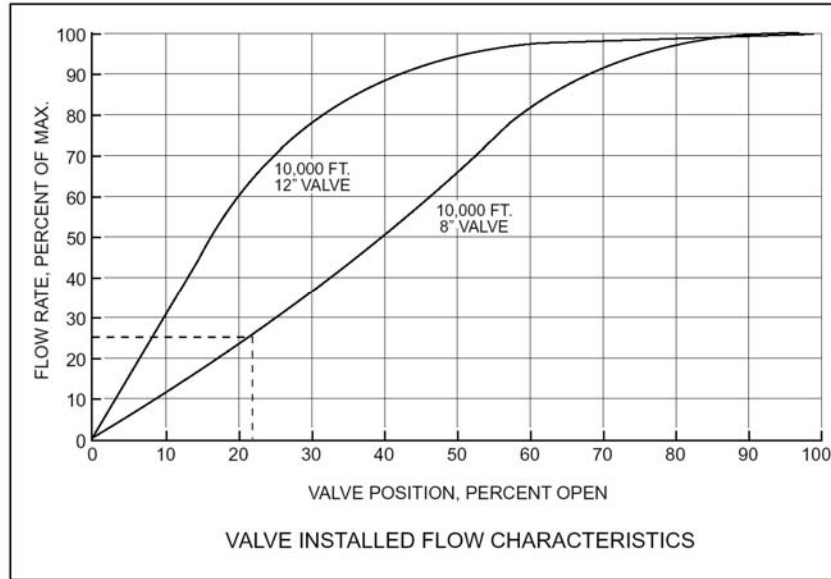


FIGURE 5. Installed Flow Characteristics By Size

CONCLUSION

Because AWWA C507 ball valves have the lowest headloss and best flow characteristic, they are the preferred valve for pump control for both water and wastewater service. Ball valves can be equipped with electric motor or hydraulic actuators for reliable pump control service.

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